

# Evaluation of Solid Sorbents as a Retrofit Technology for CO<sub>2</sub> Capture

DE-FE0004343

NETL CO<sub>2</sub> Capture Technology Meeting Pittsburgh, PA Aug. 22, 2011



# Acknowledgments



- US DOE NETL
- Stantec Consulting, Ltd.
- Shaw Energy & Chemicals, Inc.
- EPRI
- Southern Company
- Luminant













#### Presentation Outline



- Background on ADA CO<sub>2</sub> Capture Program
- Discussion of 1 MW<sub>e</sub> Pilot Project Scope and Schedule
- ADA Solid Sorbent Technology Status Update
- Q&A

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# **Development Approach**



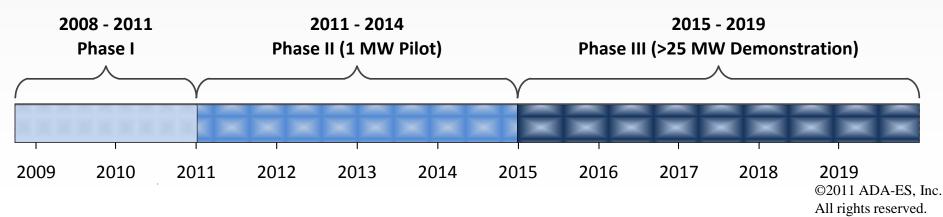
Phase I: Concept

Phase II: Pilot Testing (1 MW) Phase III: Demonstration (> 25 MW)

Commercial Implementation

- Begin with the end in mind
- Identify cost drivers
- Focus R&D and execute work schedule with commercialization goal in mind





# **ADA CO<sub>2</sub> Capture Program**



#### Phase I – Viability Assessment

- Cooperative Agreement: DE-NT0005649
  - Dual Focus: Sorbents & Process
  - 1 kW<sub>e</sub> Test Device

#### Phase II – FEED & Pilot Testing

- Cooperative Agreement: DE-FE0004343
  - Sorbent Selection
  - Full-Scale Conceptual Design
  - 1 MW<sub>e</sub> Pilot Unit
  - Techno-Economic Assessment

#### Phase III (Demonstration)

- Full-Scale Preliminary Design
- Validate Design (>25 MW<sub>e</sub>)

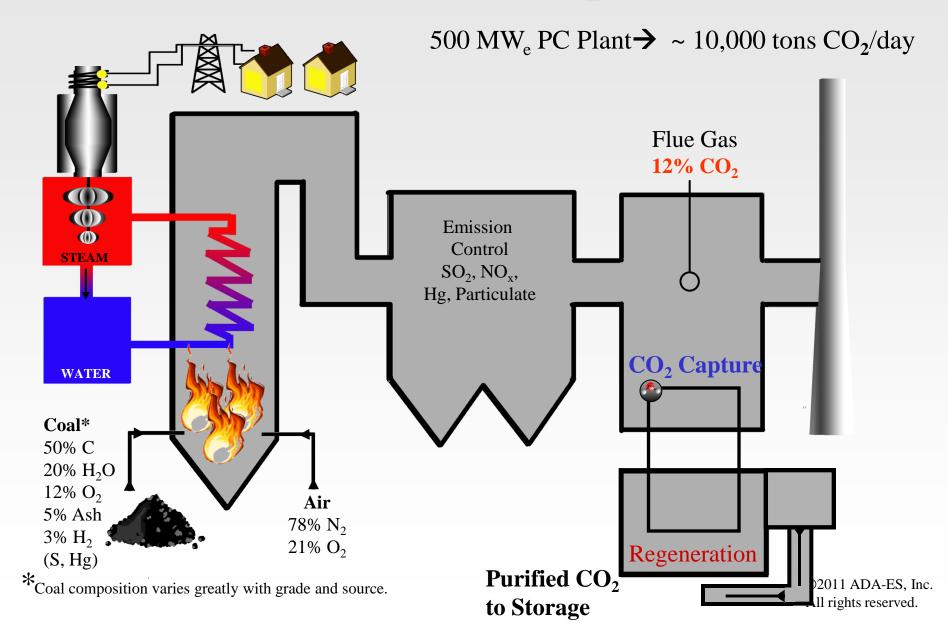




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# Post-Combustion CO<sub>2</sub> Capture





# **Technology Objectives**



- Reduction in energy penalty and costs associated with post-combustion CO<sub>2</sub> capture, compression, and sequestration
- Reduction in overall environmental impacts versus other CO<sub>2</sub> capture options
- Reliable operation
- Applicable to retrofit and new builds



# Evaluation of Solid Sorbents as a Retrofit Technology for CO<sub>2</sub> Capture



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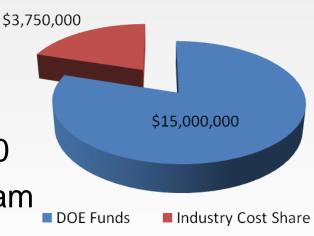


# **Project Objectives**



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- The overall objective of this funding stage is to validate solid sorbent-based post combustion CO<sub>2</sub> capture through slipstream pilot testing.
- Project Goals:
  - Achieve 90% CO<sub>2</sub> Capture
  - LCOE increase less than <35%</li>
  - Commercial deployment by 2020
  - Generate a high purity CO<sub>2</sub> stream
  - Successfully scale sorbents



Federal Funding provided by the DOE National Energy Technology Laboratory's Innovations for Existing Plants Program

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# **Project Team**



DOE – NETL

- NETL
- Project Sponsor
- ADA-ES, Inc.
  - Project Management
  - Sorbent Evaluation & Selection
  - Conceptual Process Design
  - Techno-Economic Assessment
- Shaw Energy & Chemicals, Inc.
  - Detailed Engineering Services
  - Significant Experience with Fluidized Bed Reactor Design
  - Isothermal and Adiabatic Reactors
    - Single & Multibed Reactors

- Stantec Consulting Ltd.
  - Cost Analysis



- Plant Integration
- Owners EngineerPerspective
- EPRI



- Industry Cost Share
- Independent Performance
   Evaluation and Techno Economic Assessment
- Southern Company
  - Host Site



- Cost Share
- Luminant



Cost Share

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# **Key Personnel**



#### **Project Execution**

- DOE NETL
  - Bruce Lani (Project Manager)
- ADA-ES, Inc.
  - Sharon Sjostrom (Principal Investigator)
  - Travis Starns (Project Manager)
  - Holly Krutka (Scientific Advisor)
  - Cody Wilson (Project Technical Lead)
- Shaw E&C, Inc.
  - David Adam
  - Roy Silverman
  - Robert Sandel
- Stantec Consulting Ltd.
  - Mike Richard
  - Bhurisa Thitakamol

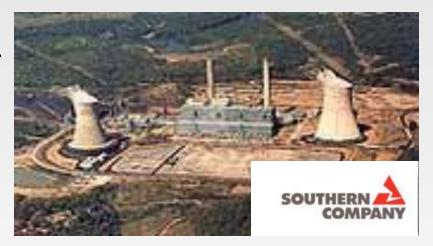
#### **Industry Participants**

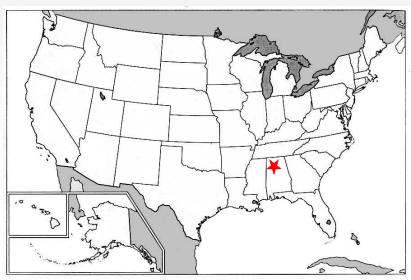
- EPRI
  - Richard Rhudy
- Southern Company
  - Michael Ivie
- Luminant
  - Rick Jeans

### **Host Site Information**



- Host Site: Southern Company –
   Alabama Power Co. Plant Miller
  - 4 EGUs (~2,640 MW<sub>e</sub>)
  - PRB Coal
  - WFGD
  - Pilot Located near WFGD on Unit 1
- Designed for 90% CO2 Capture
  - $\sim 2,100 \text{ lb CO}_2/\text{hr}$
  - Flue Gas Flow Rate ~ 3,500ACFM





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# **Project Outline**

and



# Phase I: 18 months

Refine 500 MW
 Conceptual
 Design and
 Sorbent Selection

Design 1 MW pilot

Scale down to 1 MW

Manufacture

\_\_\_\_ Construction

- Manufacture Sorbents
- Fabricate and Install 1 MW pilot

Phase III: 15 months

- 1 MW Testing
- Develop 500 MW Preliminary Design
- Conduct Technoeconomic analysis

Demonstration Phase

Phase II: 18 months

# 1 MW Pilot Schedule Summary



#### Phase I

- Task 1 Project Management Planning
- Task 2 Full-Scale Design & Sorbent Selection
- Task 3 Detailed Pilot Design

#### Phase II

- Task 4 Sorbent Procurement
- Task 5 Procure & Fabricate Pilot Equipment
- Task 6 Installation & Startup

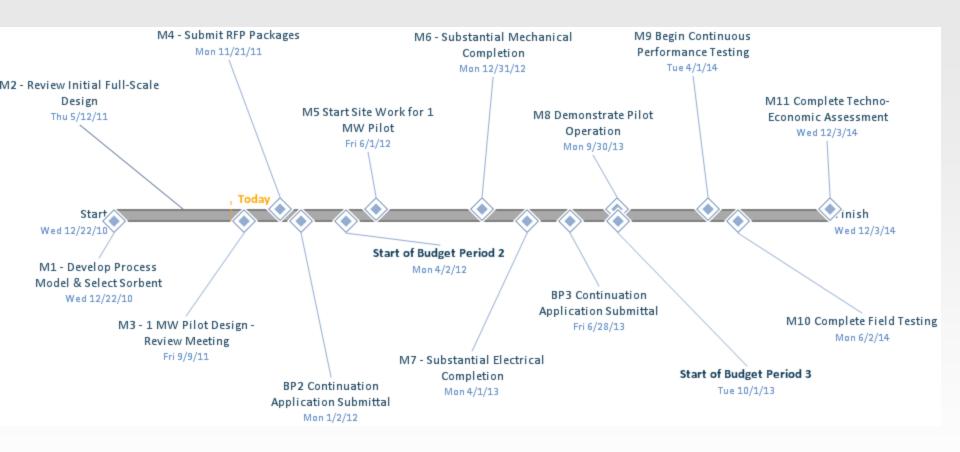
#### Phase III

- Task 7 Testing
- Task 8 Collect Sequestration Information
- Task 9 Final Reporting, Revise Design Specifications



# **Project Milestone Summary**







# **Technology Status**

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## Sorbent Selection

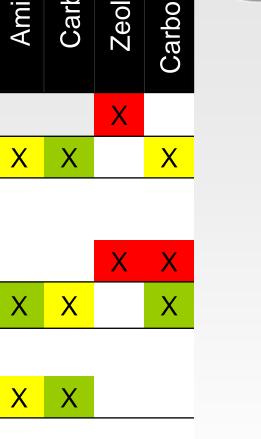
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- Effect of Moisture
- Effect of Flue Gas Constituents
- Theoretical Regeneration Energy
  - Theoretical RE
  - Working Capacity
  - ΔT<sub>ads.-regen.</sub>
- Cyclic Stability
- Rate of Reaction (qualitative)

**Promising Materials:** Supported Amines

Four supported amine sorbents produced in 600 lb quantities for 1 kW pilot testing.

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# **Promising Supported Amine Sorbents**



#### Sorbent BN

- Advantages
  - Kinetics
  - Higher working CO<sub>2</sub> capacity
  - Stability
  - Commercially available
  - Experience with changing particle size
  - Potential regeneration after the formation of heat stable salts

#### Concerns

- Particle size needs to be adjusted for process design
- Moisture uptake

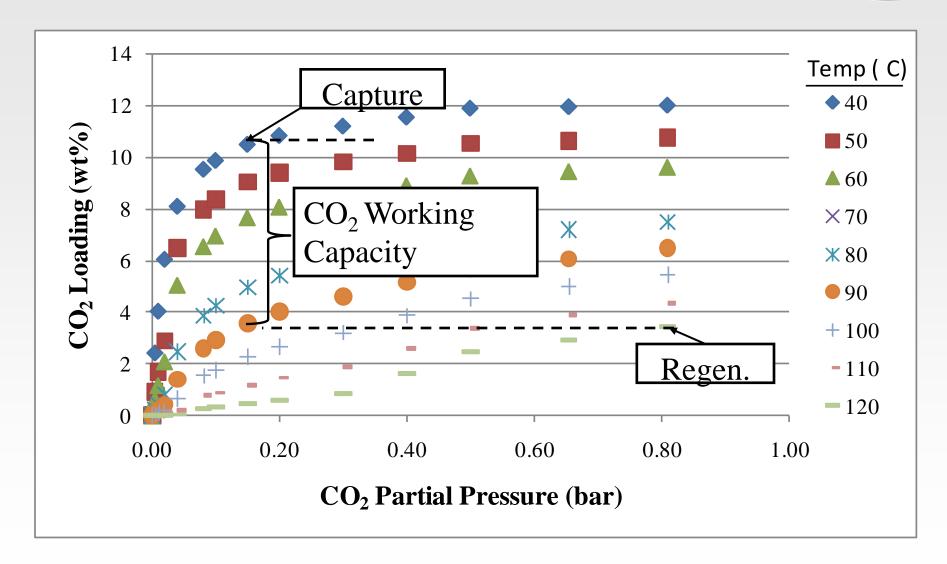
#### Sorbent CE

- Advantages
  - Extremely high total CO<sub>2</sub> capacity
  - Stability
  - Physical properties fluidized beds
- Concerns
  - Regeneration requires lower partial pressure for adequate working capacity
  - Kinetics
  - Moisture and condensation

Sorbent BN selected for use in 1 MW Pilot

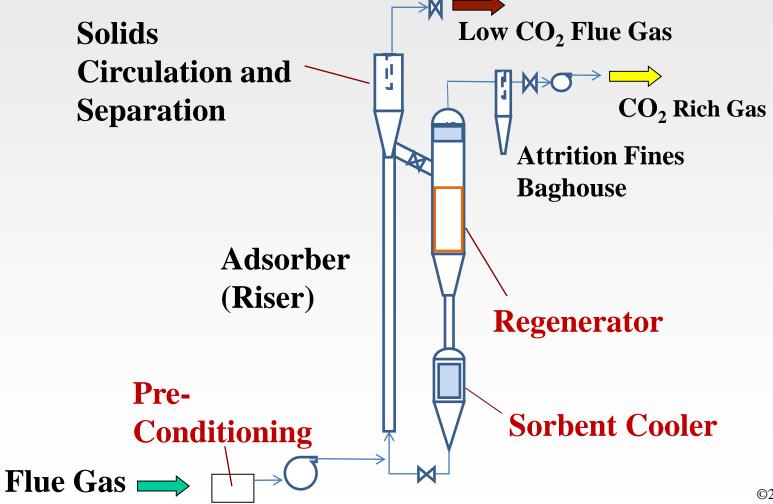
### **TGA Generated Sorbent BN Isotherms**





# 1kW<sub>e</sub> Test Device

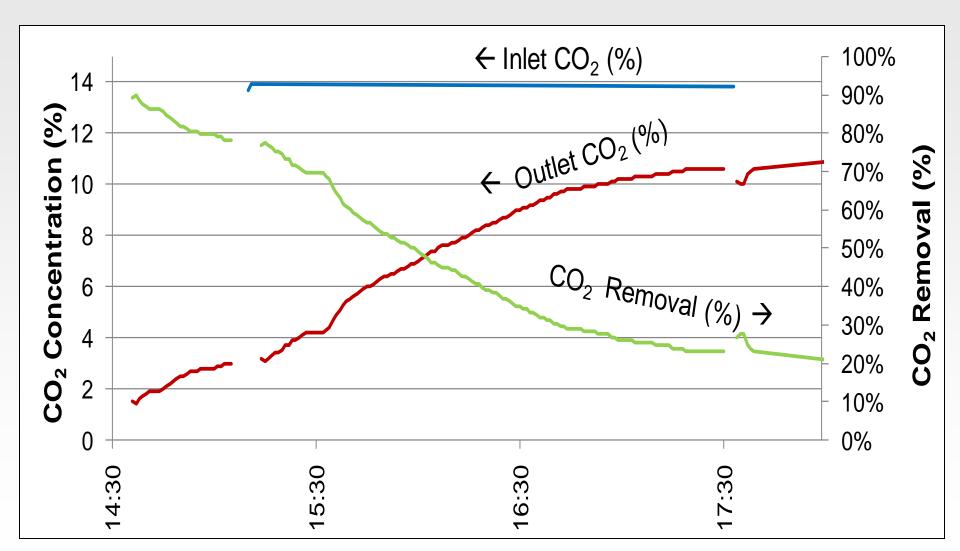


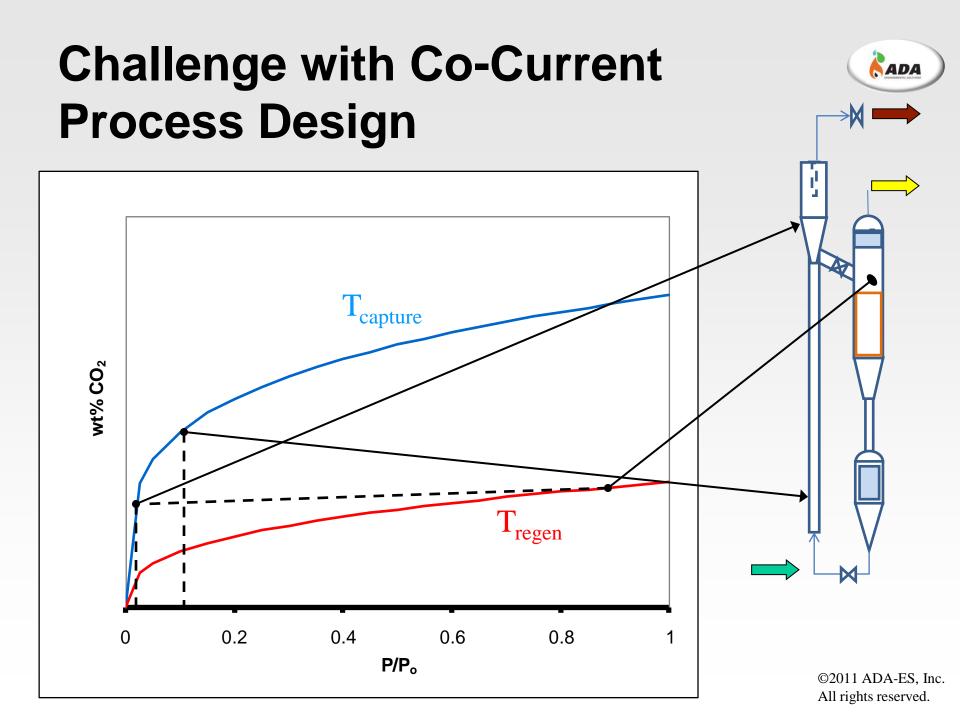


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# Continuous Testing – 1 kW<sub>e</sub> Test Device





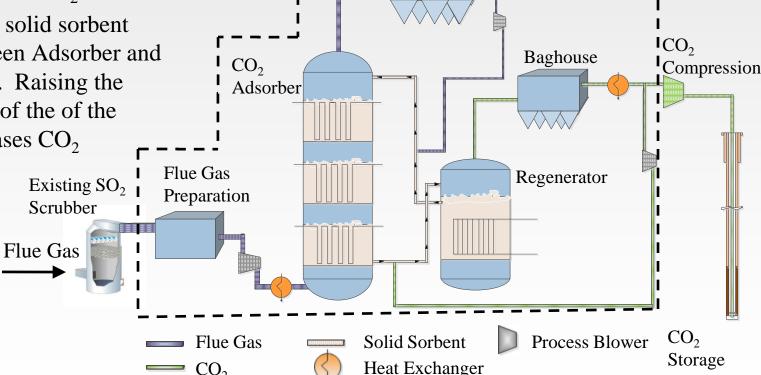


#### ADA Solid Sorbent CO2 Removal Process



## Principal

- Flue gas passes through Adsorber module where sorbent particle adsorbs CO<sub>2</sub>
- Regenerable solid sorbent cycles between Adsorber and Regenerator. Raising the temperature of the of the sorbent releases CO<sub>2</sub>



1 MW Pilot

Baghouse

Next Steps: Heat Integration & Optimization

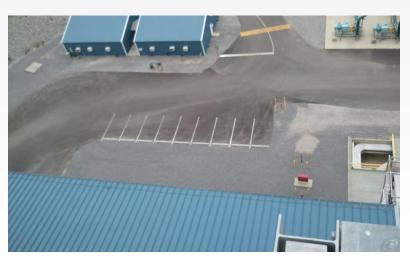
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#### 1 MW Pilot: Focus Areas



- Sorbent attrition
  - Currently using data for FCC catalysts
  - Physical & chemical
- Volatile emissions
- Validate regeneration energy requirement
- Measure actual adsorption temperatures to maintain 90% CO<sub>2</sub> capture
- CO<sub>2</sub> purity
- Sorbent regeneration time

- Process effect from flue gas constituents
  - Presence of moisture
- Optimize process variables
  - Temperatures
  - Sorbent circulation rates





# Creating a Future with Cleaner Coal

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Project Manager: Travis Starns traviss@adaes.com

Scientific Advisor: Holly Krutka hollyk@adaes.com

Project Technical Lead: Cody Wilson codyw@adaes.com

# **Task Summary**



#### Phase I

- Task 1 Project
   Management Planning
- Task 2 Refine Full-Scale Design and Sorbent Selection
- Task 3 Design Pilot Equipment

#### Phase II

- Task 1 Project
   Management Planning
- Task 4 Procure & Manufacture Sorbents
- Task 5 Procure and Construct Pilot Scale Equipment
- Task 6 Install/Startup
   Pilot Scale Equipment

#### Phase III

- Task 1 Project
   Management Planning
- Task 7 Pilot Scale
   Operation & Evaluation
- Task 8 Collect Compression and Sequestration Information
- Task 9 Prepare
   Commercial
   Conceptual Design
   and Economics

(10/1/2010 - 3/31/2012)

(4/1/2012 - 9/30/2013)

(10/1/2013 - 12/31/2014)